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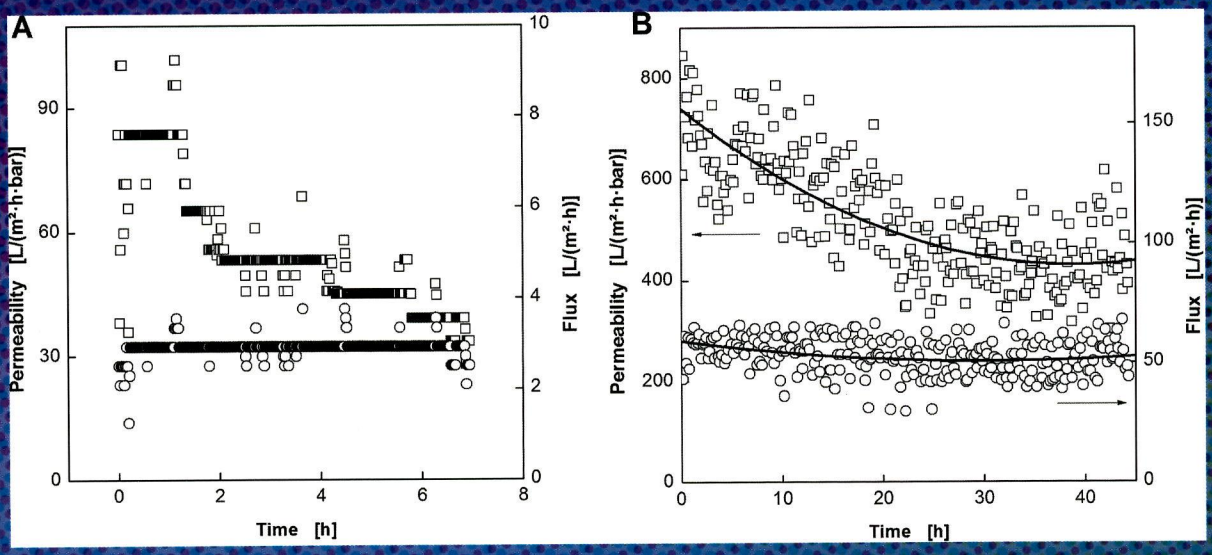

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Cover figure: Flux and permeability of fermentation suspension containing *U. maydis* cells. (A) Dead-end operation, 2.5 mL min^{-1} (DCW = ~28 g L^{-1}). (B) Reverse-flow diafiltration fitted (with V_P/V_L = 2.3; DCW = 27 g L^{-1}; air emptying); Time for feed and permeate step 60 s and for emptying and flushing step 10 s; Flow rates were 8 mL min^{-1} for the feed and 5 mL min^{-1} for the permeate step and 12.6 mL min^{-1} for emptying and flushing step. See the article "Continuous production and recovery of itaconic acid in a membrane bioreactor" by F. Carstensen et al.